

Analyzing Single-Drop Granule Formation and Strength

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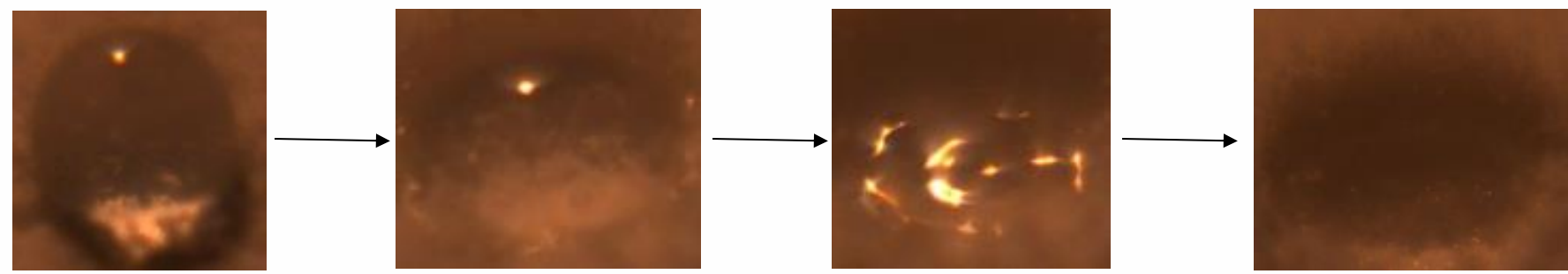
How does impact velocity and liquid binder viscosity affect the penetration time of a liquid droplet into a powder bed for wet granulation?

Introduction

Wet granulation is used widely for many applications, most notably the pharmaceutical industry. It is done typically to improve transportation properties and production efficiency.

$V_0 = \text{Drop Volume}$
 $\varepsilon = \text{Powder Bed Surface Porosity}$
 $r_{drop} = \text{Drop Radius on Powder Surface}$
 $\mu = \text{Liquid Viscosity}$
 $P_c = \text{Capillary Pressure}$
 $\tau_{CDA} = \text{Theoretical Penetration Time}$

Figure 1. Drop Penetration into a Powder Bed

$$\tau_{CDA} = V_0^2 \pi^2 \varepsilon^2 r_{drop}^4 \mu P_c \quad [1]$$


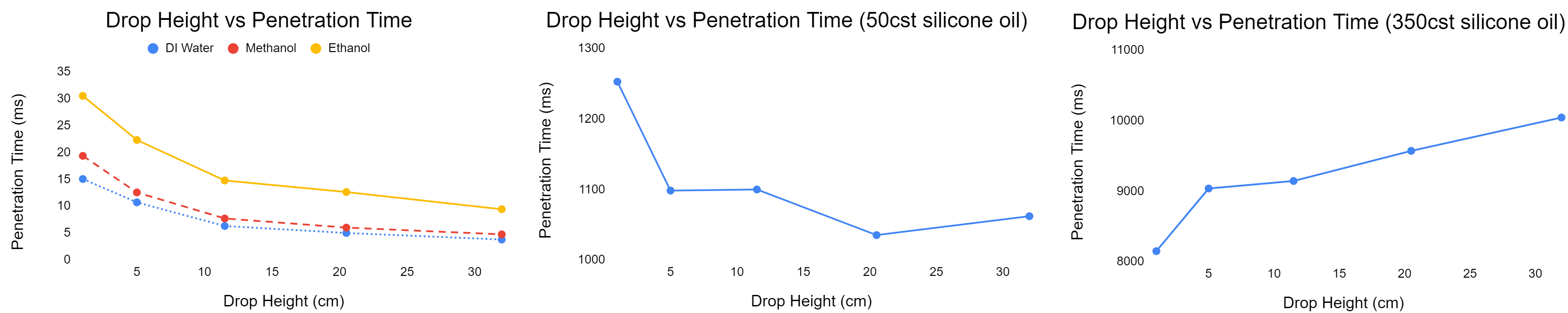
Experimental Setup

- Liquid binder dropped at set heights
- Penetration time captured with high-speed camera
- Number of frames from first impact to full absorption

Figure 2. Picture of Photron Fastcam Mini AX200



Conclusions



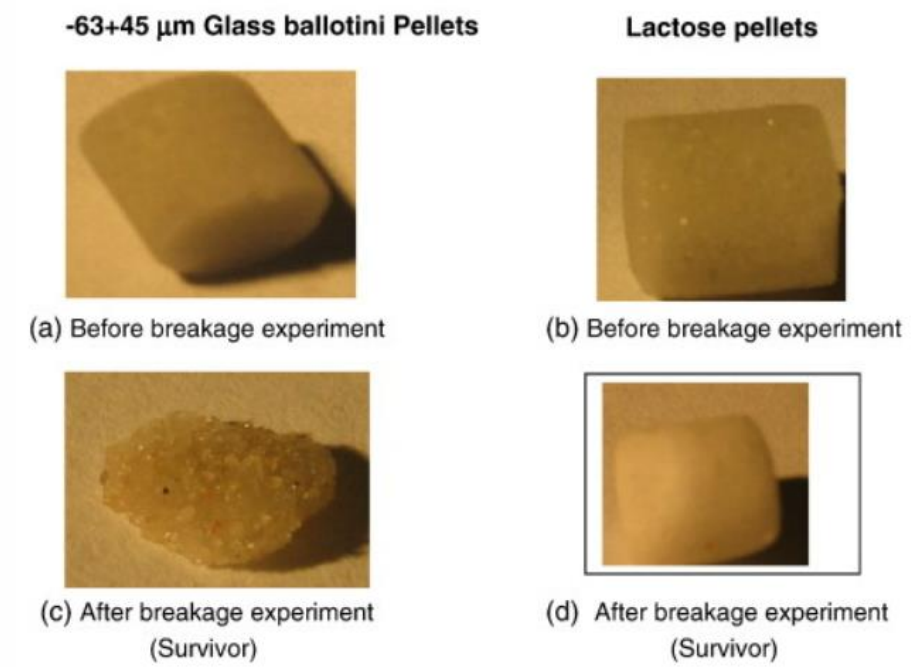
- Lower viscosity binder resulted in tunneling mechanism; Penetration time decreases with higher impact velocity.
- Higher viscosity binder led to spreading over powder surface and crater formation; Opposite correlation observed.
 - Liquid drops would initially bounce off the surface at higher viscosity/impact velocity.

How do liquid binder properties affect the breakage rate of granules in high shear mixer granulation?

Introduction

Breakage of particles allows for better dispersion of a liquid binder and limits maximum particle size. Controlling the rate of breakage allows for a more efficient process design.

Figure 3. Examples of Surviving Granules [2]



$$St_{def} = \frac{\rho_g v_c^2}{2\sigma_p} \quad [3]$$

$\rho_g = \text{Granule Density}$
 $v_c = \text{Impact Velocity}$
 $\sigma_p = \text{Granule Yield Strength}$
 $St_{def} = \text{Stokes Deformation Number}$

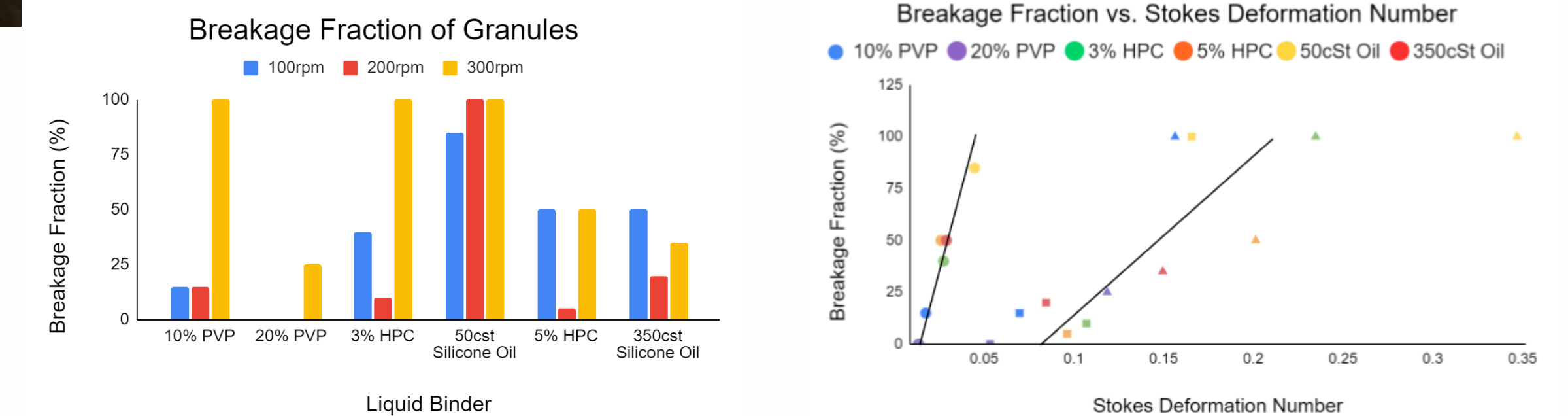
Experimental Setup



Figure 4. Picture of Key International KG5 High Shear Mixer/Granulator

- 20 granules placed into mixer bowl with carrier sand
- Number of surviving granules checked in 15 second increments for a total time of 1 minute

Conclusions



- Breakage rate depends on liquid, powder, and equipment properties, not just viscosity.
- Breakage rates follow trend lines at $St_{def} = 0.02$ and $St_{def} = 0.2$ with some outliers.

References

1. Iveson SM, Litster JD, Hapgood K, Ennis BJ. Nucleation, growth and breakage phenomena in agitated wet granulation processes: a review. *Powder Technology*. 2001;117(1-2):3-39. doi:[https://doi.org/10.1016/s0032-5910\(01\)00313-8](https://doi.org/10.1016/s0032-5910(01)00313-8)
2. Liu LX, Smith R, Litster JD. Wet granule breakage in a breakage only high-shear mixer: Effect of formulation properties on breakage behaviour. *Powder Technology*. 2009;189(2):158-164. doi:<https://doi.org/10.1016/j.powtec.2008.04.029>
3. Smith RM, Liu LX, Litster JD. Breakage of drop nucleated granules in a breakage only high shear mixer. *Chemical Engineering Science*. 2010;65(21):5651-5657. doi:<https://doi.org/10.1016/j.ces.2010.06.037>